



Enchemica, LLC
2335 Buckingham Circle
Loveland, CO 80538 USA
1-970-481-9338

DRAFT TECHNICAL MEMORANDUM

TO: Vicky Peacey, Resolution Copper

FROM: Ted Eary, Enchemica

DATE: July 17, 2018

SUBJECT: Alternative 4 - Silver King Filtered: Prediction of Operational Tailings Circuit Solute Chemistry

1 INTRODUCTION

The draft environmental impact statement (DEIS) for the Resolution Copper mine includes assessment of the following tailings storage facility alternatives:

- Alternative 1: No Action
- Alternative 2: Near West Modified Proposed Action
- Alternative 3: Near West Modified Proposed Action – Thin Lift/PAG Cell
- Alternative 4: Silver King Filtered
- Alternative 5: Peg Leg
- Alternative 6: Skunk Camp

Water balances models have been developed for each of these alternatives. These water balance models have been augmented by the addition of chemical balances. The purpose of this memo is to provide a description of the predictions of the chemical balance and resulting solute chemistry for Alternative 4.

2 MODEL SETUP

2.1 Software

The predictive model was developed with a combination of GoldSim (version 12.0) and PHREEQC (Parkhurst and Appelo, 2013; version 3.0). GoldSim was used for the water and chemical mass balance components of the model. PHREEQC was used to simulate reactive processes that affect water chemistry. The WATEQ4F.DAT thermodynamic database was used for the PHREEQC calculations. The chemical portions of the model include calculations for:

- Ca, Mg, Na, K, Cl, HCO₃, SO₄, Si, F, NO₃-N, Al, Sb, As, Ba, Be, B, Cd, Cr, Co, Cu, Fe, Pb, Mn, Mo, Ni, Se, Ag, Tl, Zn, and pH

The PHREEQC geochemical model was integrated directly into the GoldSim water balance model, so that changes to water chemistry resulting from reactive processes are made at each time step in the simulations and incorporated directly into the simulation results.

2.2 Input Data

A common set of inputs for water chemistry and flow rates from the block cave mine was used for all TSF alternatives. These inputs are described in Enchemica (2018).

2.3 Simulation Period

The simulation period was 41 years, which represents the life of mine per the mine plan of operations. A 1-day time step was used. Both the water balance and PHREEQC calculations are conducted at each time step. A 3-day timestep was found to be short enough prevent potential mass transfer warnings from GoldSim while being long enough to yield reasonably short model run times.

3 WATER BALANCE

A model of the water balance for Alternative 4 was developed by KCB (KCB, 2018). The boundaries of the KCB water balance model included the West Plant, tailings storage facility (TSF), and seepage collection systems. The details of the water balance relevant to the solute balance are provided in KCB (2018).

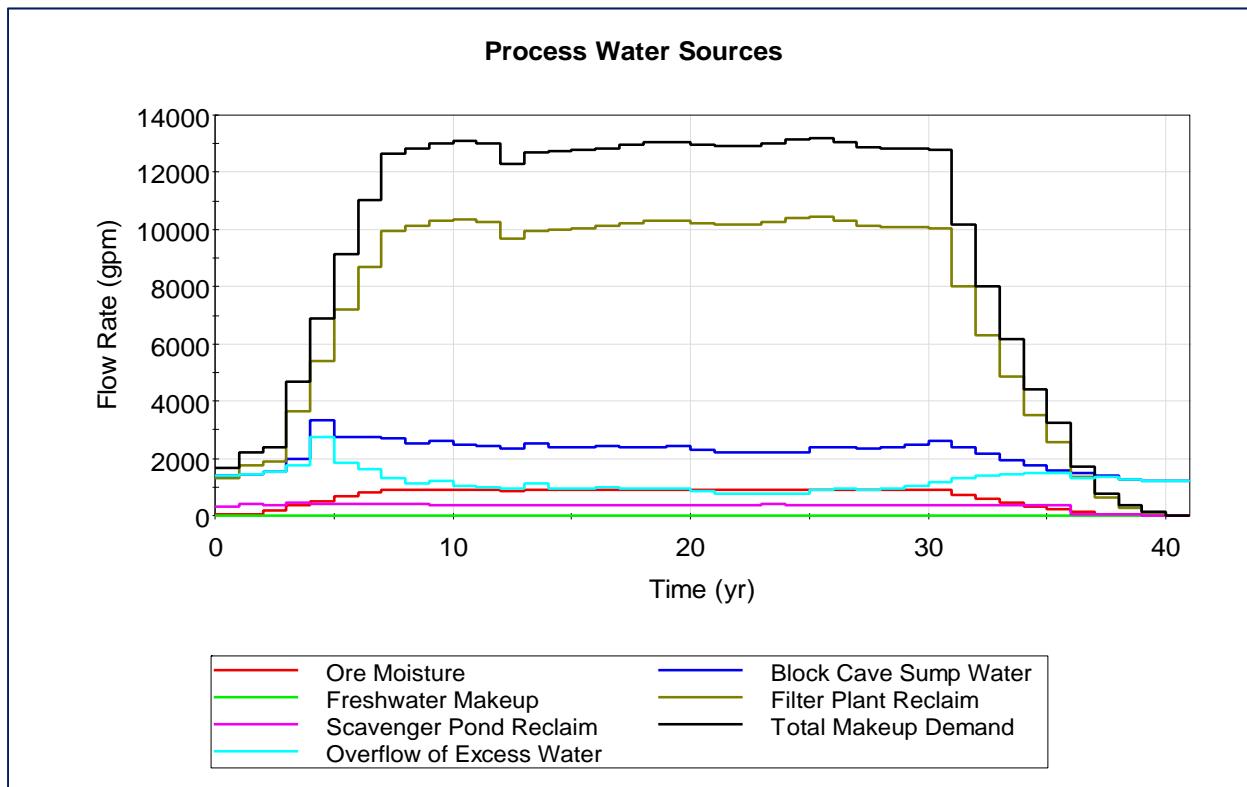
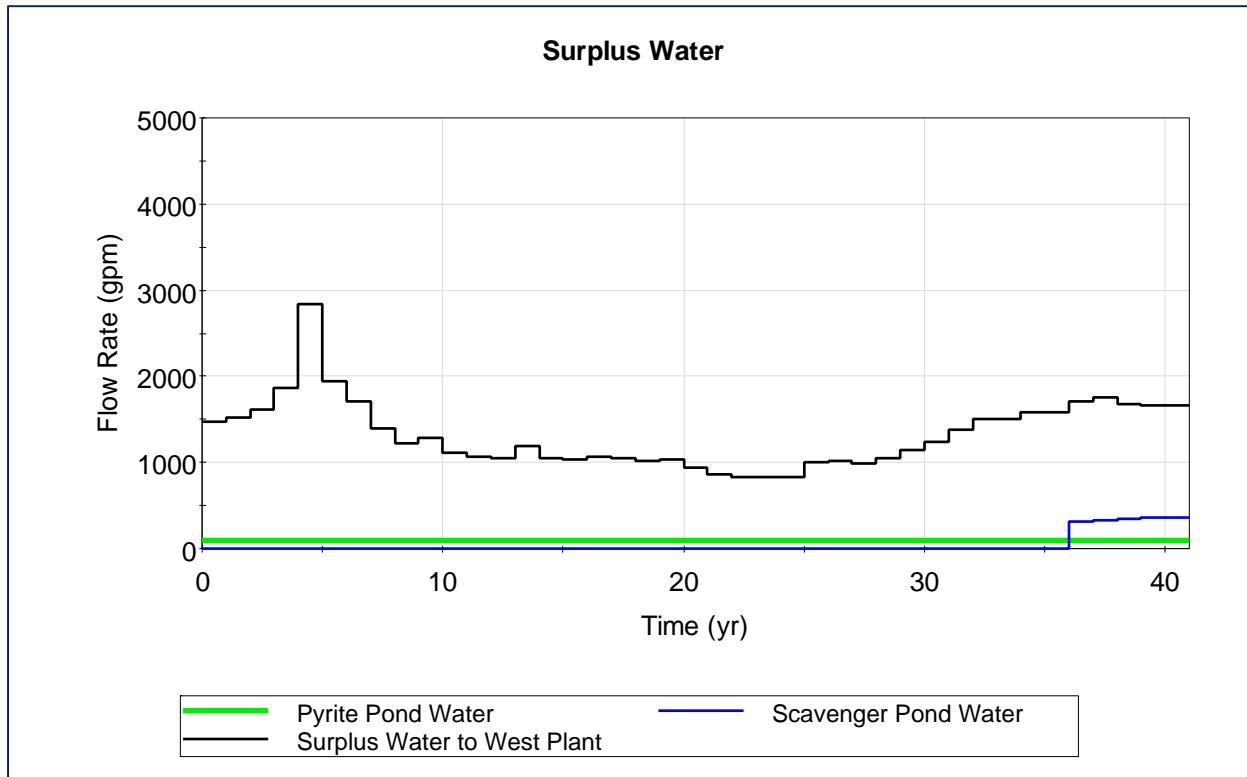
3.1 Makeup Water

The KCB water balance model provided calculations of the rate of reclaim water flow to the West Plant and the total demand for additional makeup water needed for ore processing at the West Plant. There are five sources of water for ore processing:

- **Reclaim water:**
 - **Scavenger Pond Reclaim:** Excess water pumped from the Scavenger Pond – this flow is provided by the KCB water balance model.
 - **Filter Plant Reclaim:** Water returned from filtering of tailings – this flow is provided by the KCB water balance model.
- **Makeup water:**
 - **Ore moisture:** Ore entering the West Plant is estimated to contain 4% by weight of water.
 - **Block cave sump water:** The block cave mine is expected to have an excess amount of water that will be pumped to the surface providing a source of makeup water.
 - **Freshwater:** The demand for makeup water in exceedance of reclaim and flows from the block cave mine will be comprised of a mixture of freshwater from the Central Arizona Project canal and well fields.

Figure 3-1 shows simulation results for process water sources. Reclaim from the filter plant is the largest source of water for ore processing followed by block cave sump water, ore moisture, and scavenger pond reclaim. There is a surplus of water from the sources listed above throughout the operational mine life as shown by the overflow of excess water in Figure 3-1 (KCB, 2018).

Figure 3-2 shows a simulation specifically for surplus water. The surplus water to the West Plant is comprised of filter plant reclaim and block cave water. Additional sources of surplus water include excess water from the Pyrite Pond that cannot be used for ore processing because of very poor water quality (Duke, 2017), and starting at about year 35 when ore processing ramps down, excess water from the Scavenger Pond. Flow of excess water from the Pyrite Pond is predicted to average about 90 gpm. Flow of excess water from the Scavenger Pond is predicted to average about 350 gpm after year 35.

**Figure 3-1. Simulation results for process water sources****Figure 3-2. Surplus water requiring management**

4 CALCULATION SEQUENCE FOR SOLUTE CHEMISTRY

The calculation sequence in the solute model is:

- Chemical loads are defined for all water sources entering the TSF system by multiplication of flow rates times concentrations. Descriptions of the source water chemistries are in Enchemica (2018).
- The chemical loads are converted to concentrations at locations of water mixing and storage.
- The concentrations are equilibrated with PHREEQC for aqueous speciation, solubility, and adsorption. The set of equilibria processes for PHREEQC are described in Enchemica (2018). There are five locations where PHREEQC is applied to produce equilibrated water chemistries:
 - **West Plant:** mixture of water entering the Plant
 - **Pyrite Tailings:** water contained in the pore space of deposited pyrite tailings
 - **Pyrite Pond:** water collected from the pyrite tailings and associated runoff areas. Water in this pond is not used as a reclaim to the West Plant due to very poor quality.
 - **Lost Seepage from Pyrite Tailings and Pyrite Pond:** combined flow of water predicted to seep from deposited pyrite tailings and pond.
 - **Scavenger Tailings/Embankment:** water contained in the pore space of deposited scavenger tailings.
 - **Scavenger Pond:** storage of water collected from the scavenger tailings and associated runoff areas. This pond is used as a reclaim water source for the West Plant.
 - **Lost Seepage from Scavenger Tailings/Embankment and Scavenger Reclaim Pond:** combined flow of water predicted to seep from deposited scavenger tailings and pond.
 - **Surplus Water:** The water balance indicates there would be excess water from the Pyrite Pond and other makeup sources.
- Equilibrated water chemistries are multiplied by flow rates to move chemical loads through the water distribution system.

The water balance model indicates four points of seepage that have the potential to bypass collection systems. These are:

- Scavenger Tailings/Embankment and Scavenger Pond – combined Lost Seepage
- Pyrite Tailings and Pyrite Pond – combined Lost Seepage

The two potential seepages from each of these combined sources are used to provide an estimate of the chemical compositions for the two types of lost seepage predicted to occur from the pyrite and scavenger TSFs. The pyrite pond will be lined and is predicted to have a low rate of (up to 1.3 gpm) but influences seepage chemistry due to its high chemical load.

Reactions and mixing of Lost Seepage with groundwater in flow paths from the TSF are not included in the modeling logic. Transport of Lost Seepage along flow paths is the subject of associated modeling studies by Montgomery and Associates.

5 RESULTS

A full set of results from the model are provided in tables below as annual average concentrations. The tables are organized as follows:

- Table 5-1: Pyrite Pond
- Table 5-2: Combined lost seepage from the Pyrite Pond and Pyrite Tailings
- Table 5-3: Combined lost seepage from the Scavenger Pond Scavenger Tailings
- Table 5-4 Predictions of average annual concentrations for Surplus Water: Surplus Water

5.1 Pyrite Pond and Tailings

Examples of model results are shown in Figure 5-1 for the Pyrite Pond and Figure 5-2 for lost seepage combined for the Pyrite Pond and Pyrite Tailings. The data in these charts are average annual concentrations for the 41-year operational mine life. The following observations are made from the predictions of Pyrite Pond chemistry:

- Figure 5-1a - pH: The pH is predicted to be acidic in the range of 2.8 to 3.0 for the entirety of the 41-year operational mine life.
- Figure 5-1b – major anions: Sulfate is the dominant anion at concentrations up 18,700 mg/L. Fluoride is next in importance with concentrations up to 280 mg/L. The predicted concentrations for chloride and nitrate-N are lower typically less than 15 mg/L and 3 mg/L, respectively.
- Figure 5-1c – divalent metals: Copper is predicted to have the highest concentrations, ranging up to 2160 mg/L. Concentrations of nickel, cobalt, and zinc are predicted to range from about 10 to 20 mg/L. Concentrations of cadmium and lead are predicted range up to 0.07 and 0.006 mg/L, respectively.
- Figure 5-1d: anionic metals and metalloids: Molybdenum concentrations are the highest for this group at concentrations up to about 0.5 mg/L. Arsenic is next highest at concentrations up to about 0.4 mg/L followed by selenium at concentrations up to about 0.2 mg/L. Antimony concentrations are predicted to be the lowest in this group at concentrations up to about 0.0005 mg/L.

The acidic, high metal concentrations predicted for the Pyrite Pond are due to runoff from the deposited tailings. The chemistry of runoff is represented by measured data from barrel tests conducted with samples of filtered tailings, which consistently produced leachates with low pH and high sulfate and metal concentrations (Duke, 2017).

A set of model predictions for combined lost seepage from the Pyrite Pond and Pyrite Tailings is shown in Figure 5-2. Seepage from the Pyrite Pond is acidic with high metal loads, but it is expected to have a very low flow due to placement of a liner under the pond. Seepage from the Pyrite Tailings is process water, but it is expected to have a higher flow rate than seepage from the Pyrite Pond. The following observations are made from the predictions of combined lost seepage from the Pyrite Pond and Pyrite Tailings:

- Figure 5-2a - pH: The pH is predicted to drop over time from 6.4 to 5.2 as the acidity of the Pyrite Pond increases over the 41-year operational mine life and mixes with the pyrite tailings seepage.
- Figure 5-2b – major anions: Sulfate is the dominant anion at concentrations from 670 to 2240 mg/L Chloride is next highest at concentrations up to 100 mg/L. Bicarbonate concentrations are predicted to be 0 mg/L and fluoride is in the range of 3 to 14 mg/L. Nitrate-N concentrations are predicted to be in the range of 2 to 4 mg/L.

- Figure 5-2c – divalent metals: Copper is predicted to have the highest concentrations, ranging up to 78 mg/L. Zinc is next highest, ranging up to 3.2 mg/L. Concentrations of cobalt and nickel are approximately the same at concentrations from 0.1 to 0.9 mg/L. Concentrations of cadmium and lead are predicted range up to 0.02 and 0.001 mg/L, respectively.
- Figure 5-2d: anionic metals and metalloids: Molybdenum concentrations are the highest for this group at concentrations up to about 1 mg/L. Selenium is next highest at concentrations up to about 0.27 mg/L followed by arsenic and antimony concentrations up to about 0.016 and 0.008 mg/L, respectively.

A set of model predictions for lost seepage combined for the Scavenger Tailings and Scavenger Pond is shown in Figure 5-3. The following observations are made from these predictions for combined lost seepage:

- Figure 5-3a - pH: The pH is predicted remain approximately constant at 7.6 to 7.9 over the 41-year operational mine life.
- Figure 5-3b – major anions: Sulfate is the dominant anion at concentrations from 900 to 1520 mg/L Chloride is next highest at concentrations up to 106 mg/L. Bicarbonate concentrations are predicted to range from 15 to 20 mg/L and fluoride from 2.2 to 2.4 mg/L. Nitrate-N concentrations are predicted to be in the range of 3 to 4.5 mg/L.
- Figure 5-3c – divalent metals: Zinc is predicted to have the highest concentrations, ranging up to 2.7 mg/L. Concentrations of copper, nickel, cobalt are predicted to range from about 0.1 to 0.2 mg/L. Concentrations of cadmium and lead are predicted range up to 0.01 and 0.001 mg/L, respectively.
- Figure 5-3d: anionic metals and metalloids: Molybdenum concentrations are the highest for this group at concentrations up to about 1 mg/L. Selenium is next highest at concentrations up to about 0.3 mg/L followed by arsenic and antimony concentrations up to about 0.002 and 0.008 mg/L, respectively.

5.2 Treatment of Surplus Water from the Pyrite Pond

The Pyrite Pond is predicted to fill to capacity, yielding surplus water that cannot be used for ore processing because of its expected high acidity. This acidic surplus water will need to be treated. Using the average water chemistry predicted for year 26 for the Pyrite Pond (Table 5-4) and an average flow of 90 gpm for surplus water from the Pyrite Pond, estimates for treatment parameters are:

- Lime (as $\text{Ca}(\text{OH})_2$) requirement to raise the pH from 2.9 to 9 is 11.9 g/L or 2340 tons/yr at 90 gpm. The assumptions for this calculation are 96% purity for hydrated lime, reaction efficiency of 0.8 (Cravotta et al. 2010), and the anticipated need to obtain a pH of 9 for removal of Mn and Zn. Also, it is assumed that the surplus water from the Pyrite Pond would be treated as a separate flow rather than being combined with surplus water from the Scavenger Pond and block cave mine.
- The TDS is predicted to be reduced from 21,118 mg/L to 5200 mg/L in treated water with SO_4 being the primary solute at 3830 mg/L.
- Sludge generation is estimated to be 28.2 g/L or 5570 ton/yr based on a PHREEQC calculation of precipitation of secondary minerals. The primary precipitants are gypsum, $\text{Fe}(\text{OH})_3$, $\text{Al}(\text{OH})_3$, and $\text{Cu}(\text{OH})_2$. Sludge generation during the mine operational period of 41 years would be 228,370 tons. Sludge generation for a 200-year post-closure period would be an additional 1.114×10^6 tons.

The above calculations are based on treatment with lime to provide estimates for the potential capacity needed for water treatment and sludge disposal. Other water treatment methods would have different requirements and results.

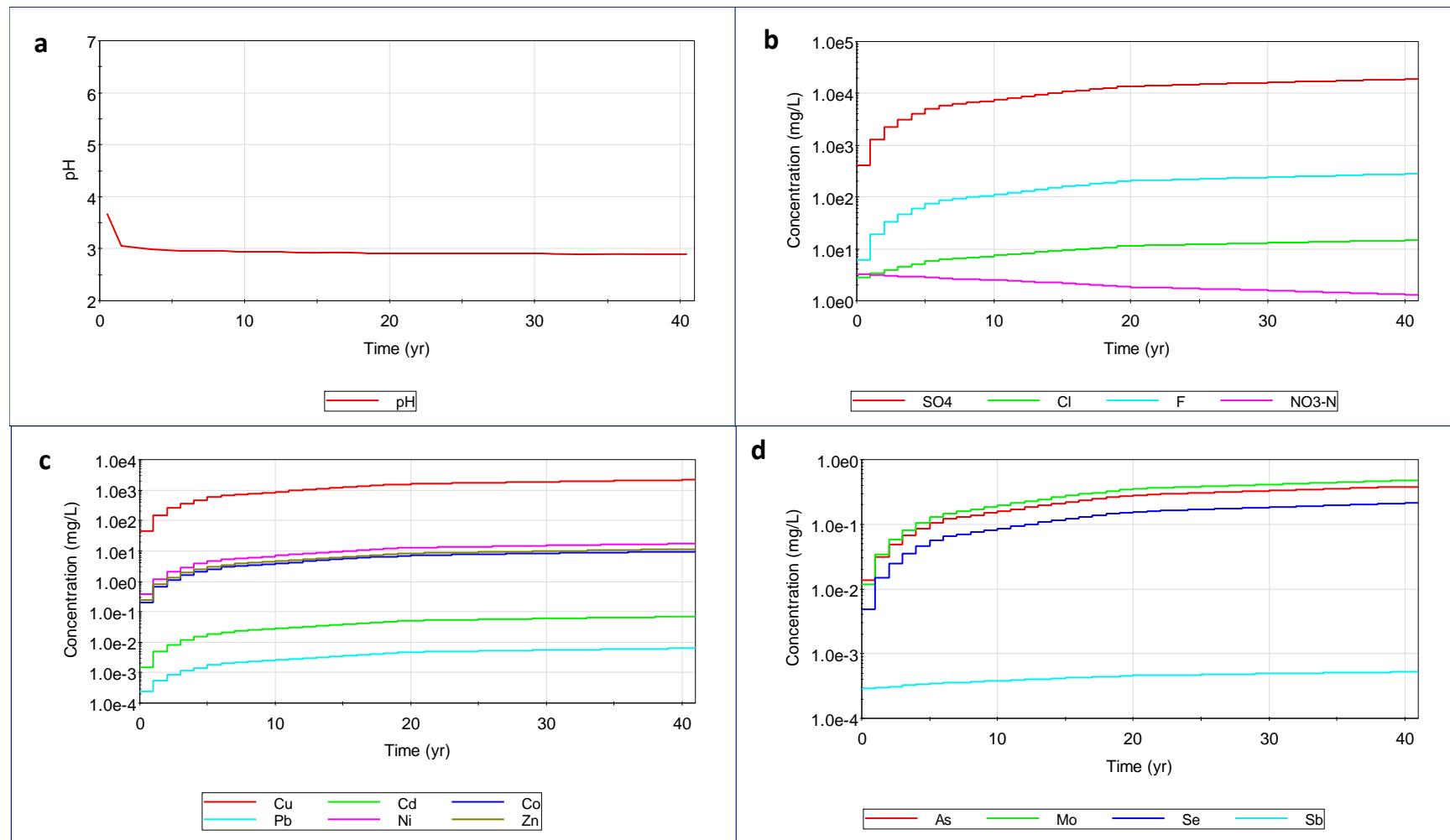


Figure 5-1. Predictions of average annual concentrations in the Pyrite Pond for a) pH, b) major anions, c) divalent metals, and d) anionic metals/metalloids

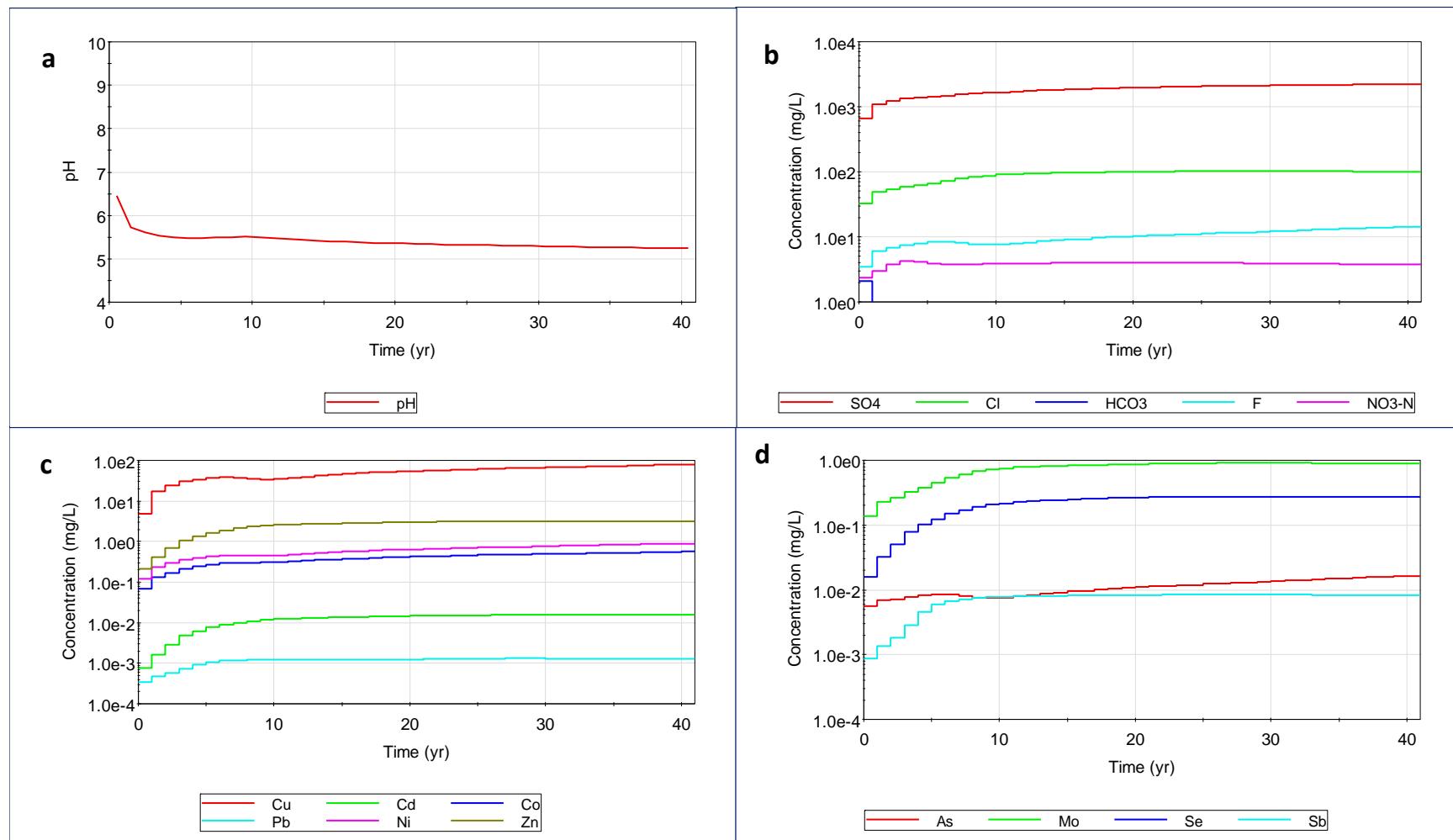


Figure 5-2. Predictions of average annual concentrations in lost seepage combined from the Pyrite Pond and Pyrite Tailings for a) pH, b) major anions, c) divalent metals, and d) anionic metals/metalloids

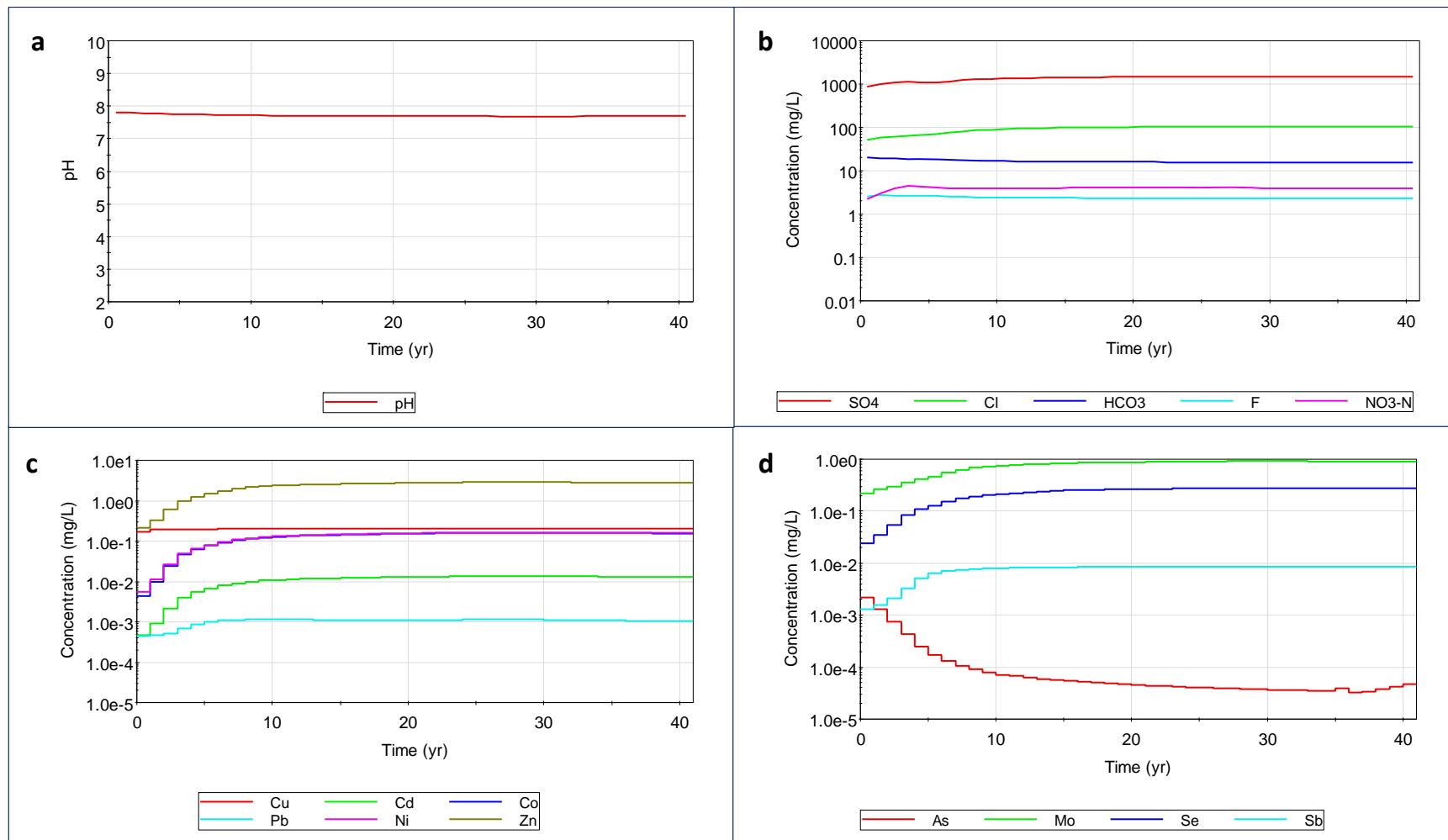


Figure 5-3. Predictions of average annual concentrations in lost seepage combined from the Scavenger Pond and Scavenger Tailings for a) pH, b) major anions, c) divalent metals, and d) anionic metals/metalloids

6 REFERENCES

Cravotta, C.A., D.L. Parkhurst, B. Means, R. McKenzie, H. Morris, and W. Arthur (2010) A geochemical module for "AMDTreat" to compute caustic quantity, effluent quality, and sludge volume. 2010 National Meeting of the American Society of Mining and Reclamation, Pittsburgh, PA Bridging Reclamation, Science and the Community June 5 - 11, 2010. R.I. Barnhisel (Ed.) Published by ASMR, 3134 Montavesta Rd., Lexington, Kentucky.

Enchemica (2018) Water Chemistry Inputs for Operational Models of Tailings Circuit Solute Chemistry. Draft Technical Memo from T. Eary (Enchemica) to V. Peacey (Resolution Copper), July 18, 2018.

KCB (2018) DEIS Design for Alternative 4 – Silver King Filtered, Draft Technical Memorandum, Klohn Crippen Berger, May 4, 2018.

Parkhurst, D.L. and Appelo, C.A.J. (2013) Description of Input and Examples for PHREEQC Version 3 – A Computer Program for Speciation, Batch-Reaction, One-Dimensional Transport, and Inverse Geochemical Calculations. U.S. Geological Survey Techniques and Methods, Book 6, Chapter A43, 497 p, available only at <http://pubs.usgs.gov/tm/06/a43>.

Duke (2017) Geochemical Reactivity of Unsaturated Pyrite Tailings. Memo from K. Duke (Duke HydroGeochem) to H. Gluski (Resolution) and M. Wickham (Wickham GeoGroup), March 3, 2017.



102 Magma Heights – P.O. Box 1944
Superior, AZ 85173
Tel.: 520.689.9374
Fax: 520.689.9304

July 20, 2018

Ms. Mary Rasmussen
US Forest Service
Supervisor's Office
2324 East McDowell Road
Phoenix, AZ 85006-2496

Subject: Response to Analysis Data Request #1 – Request for Analysis of Tailings Seepage – Item #2 Tailings Solute Modeling.

Dear Ms. Rasmussen,

In partial response to your letter dated March 8, 2018, the following documents are attached as requested:

2. Tailings Solute Modeling: It is our understanding that the water balance and geochemical modeling for tailings solute is being updated, specific to each alternative tailings storage facility, and including specific analysis of oxidation potential of the embankment. There is an expectation that modeling would cover both operational and post-closure time frames.

Request: RCM to provide USFS with block cave geochemical modeling.

RCM Response: As requested, please see the attached technical memorandums by Enchemica dated July 17, 2018 for the following tailing storage facilities (TSF):

- *Alternative 2 - Near West Modified Proposed Action: Prediction of Operational Tailings Circuit Solute Chemistry*
- *Alternative 3 - Near West Modified Proposed Action – Thin Lift/PAG Cell: Prediction of Operational Tailings Circuit Solute Chemistry*
- *Alternative 4 - Silver King Filtered: Prediction of Operational Tailings Circuit Solute Chemistry*
- *Alternative 5 - Peg Leg: Prediction of Operational Tailings Circuit Solute Chemistry*
- *Alternative 6 - Skunk Camp: Prediction of Operational Tailings Circuit Solute Chemistry*
- *Common Inputs Common to All Operational Models of Tailings Circuit Solute Chemistry*

Overall, there are no substantive differences in predictive solute chemistry for the alternative TSF sites with the exception of Alternative 4 (Silver King). The solute balances are useful tools for TSF



alternatives comparison, but it is also worth noting that the model likely over predicts solute chemistry due to several conservative assumptions:

1. No mitigations have been applied to the water chemistry
2. Water from the block cave mine, which has the poorest water quality and highest solute load, has first priority to meet the water demand at the West Plant (concentrator).
3. Makeup water needed at the end of the operational period are sourced from the Pyrite Pond and water from the block cave. The decrease in the amount of freshwater makeup results in less dilution of the combined effects of evaporation and inflow of chemical loads from the block cave.

Once a selected TSF has been identified, additional mitigation approaches may be incorporated as needed.

Sincerely,

A handwritten signature in blue ink that reads "Vicky Peacey".

Vicky Peacey,

Senior Manager, Environment, Permitting and Approvals; Resolution Copper Company, as Manager of Resolution Copper Mining, LLC

Cc: Ms. Mary Morissette; Senior Environmental Specialist; Resolution Copper Company

Enclosure(s)

Technical Memorandum by Enchemica (2018), *Alternative 2 - Near West Modified Proposed Action: Prediction of Operational Tailings Circuit Solute Chemistry*

Technical Memorandum by Enchemica (2018), *Alternative 3 - Near West Modified Proposed Action – Thin Lift/PAG Cell: Prediction of Operational Tailings Circuit Solute Chemistry*

Technical Memorandum by Enchemica (2018), *Alternative 4 - Silver King Filtered: Prediction of Operational Tailings Circuit Solute Chemistry*

Technical Memorandum by Enchemica (2018), *Alternative 5 - Peg Leg: Prediction of Operational Tailings Circuit Solute Chemistry*

Technical Memorandum by Enchemica (2018), *Alternative 6 - Skunk Camp: Prediction of Operational Tailings Circuit Solute Chemistry*

Technical Memorandum by Enchemica (2018), *Common Inputs Common to All Operational Models of Tailings Circuit Solute Chemistry*